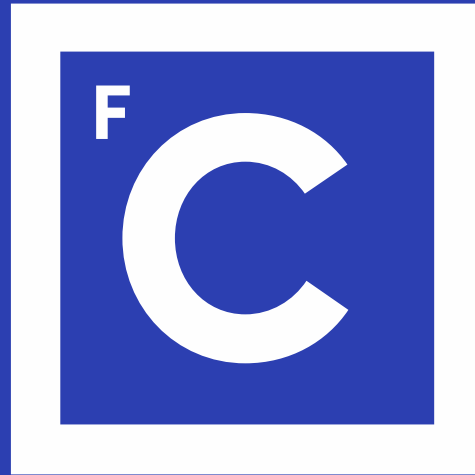




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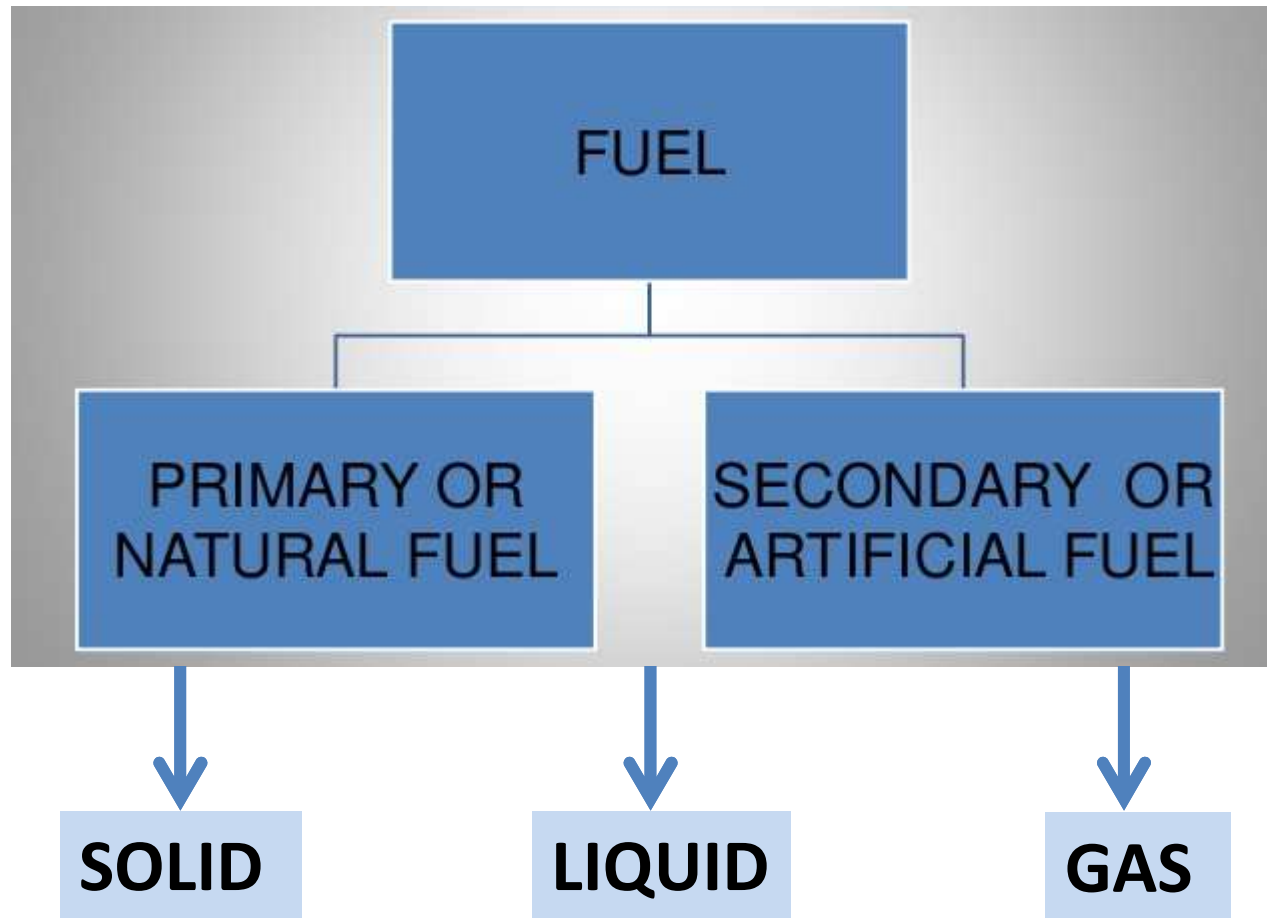
DISCIPLINA MIEA 2018



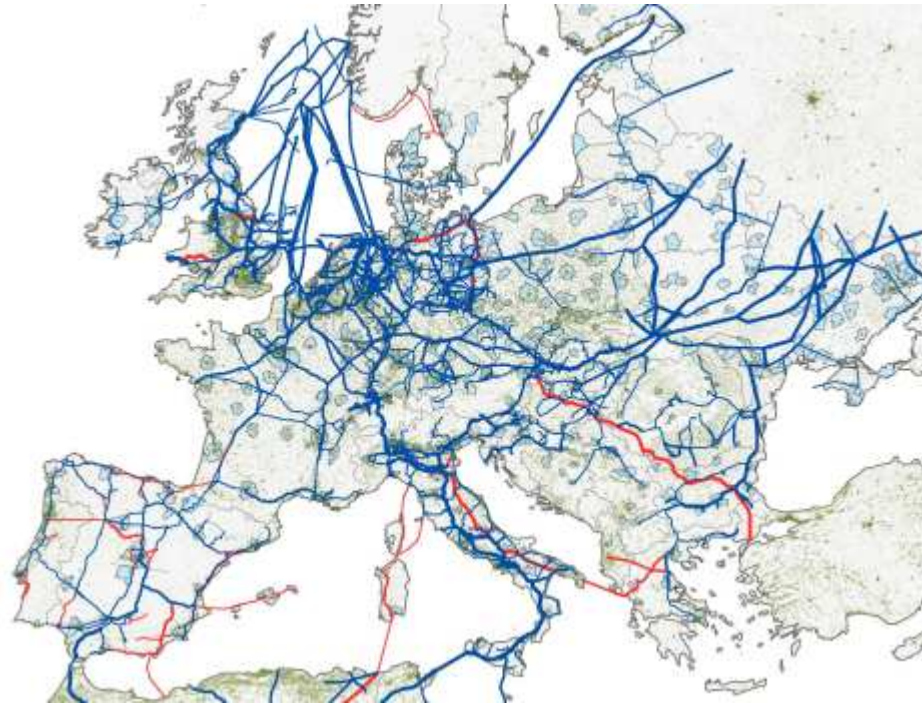
Technologies of combustion

Corpo docente

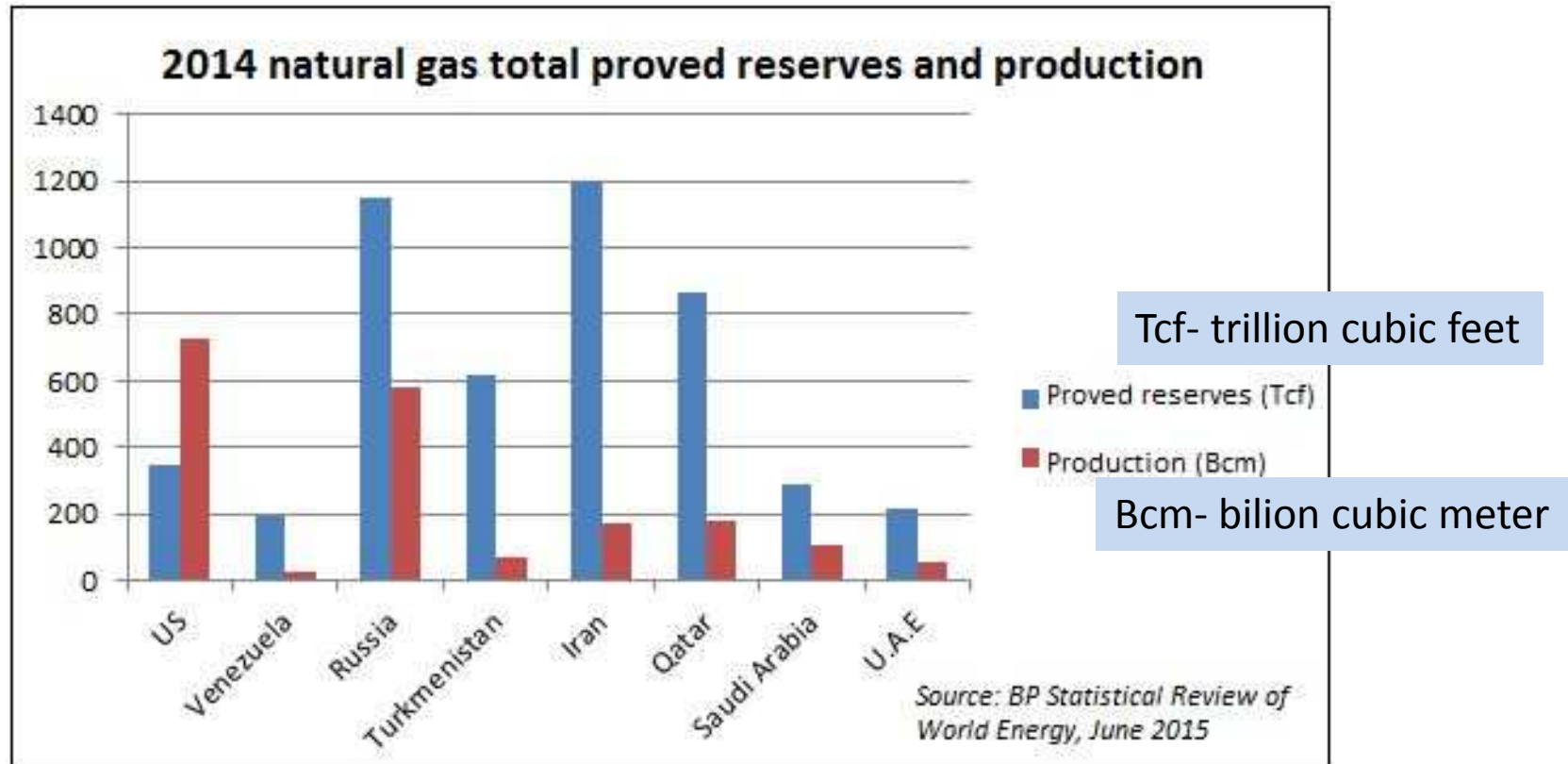
Carla Silva (Teóricas e práticas) /Theory and practice
camsilva@ciencias.ulisboa.pt



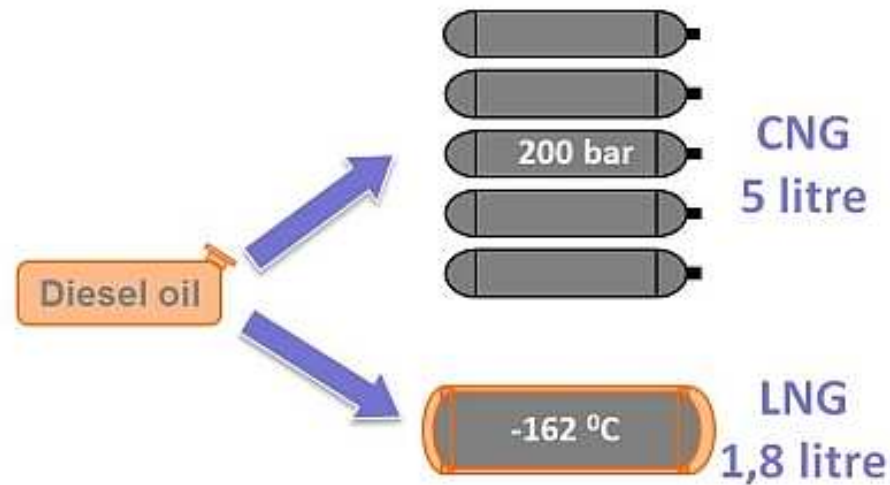
Natural gas network



**The European natural gas network.
The existing network is shown in
blue; planned pipelines in red.
Population density is represented in
dark green; larger urban areas are
coloured light blue.
(Image: ETH Zurich)**



Visual comparison of the volumetric equivalence between diesel, CNG, and LNG for a given energy content. (NGVA Europe).



Addition of odorants to help identify NG in case of a leak.

Quality/unit	Natural methane	LPG propane	LPG butane
Chemical formula	CH ₄	C ₃ H ₈	C ₄ H ₁₀
Boiling point	−162°C	−42°C	−2°C
Specific gravity of liquid fuel	–	0.5	0.57
Specific gravity of gas vapour	0.58	1.78	2.0
Gross calorific value	38.5 MJ/m ³	95 MJ/m ³	121.5 MJ/m ³
Gas family	2nd	3rd	3rd
Flammability limits	5–15%	2.3–9.5%	1.9–8.5%
Air/gas ratio	9.81:1	23.8:1	30.9:1
Oxygen/gas ratio	2:1	5:1	6.5:1
Flame speed	0.36 m/s	0.46 m/s	0.38 m/s
Ignition temperature	704°C	530°C	500°C
Max. flame temperature	1000°C	1980°C	1996°C
System operating pressure	21 ± 2 mbar	37 ± 5 mbar	28 ± 5 mbar
Liquid storage vapour pressure	–	6–7 bar	1.5–2 bar



Correlation for natural gas heat capacity developed

GAS COMPOSITIONS USED FOR GENERATING C_p VALUES Table 1

Component	Natural gas mixtures, mole %				
	Gas				
	A	B	C	D	E
CH_4	94.4	88.9	83.2	78.0	74.9
C_2H_6	2.6	5.2	8.8	10.5	10.1
C_3H_8	2.0	3.7	4.2	6.5	7.2
i- C_4H_{10}	0.5	0.7	1.1	1.5	2.4
n- C_4H_{10}	0.5	0.7	1.1	1.5	2.4
i- C_5H_{12}	0.0	0.4	0.8	1.0	1.5
n- C_5H_{12}	0.0	0.4	0.8	1.0	1.5
Mol wt	17.39	18.83	20.28	21.72	23.18
SG	0.60	0.65	0.70	0.75	0.80

Biogas		Landfill gas	Waste water treatment digester	House hold waste digester	Industrial waste/animal manure digester
Methane	vol. %	36–52 ^a	65 ^a	65 ^a	60–80/50–70 ^b
Carbon dioxide	vol. %	30–41 ^a	33.5 ^a	29 ^a	20–40/30–50 ^b
Water vapour	vol. %	0.1–3.3 ^a	2 ^a	0.5 ^a	1–4 ^b
Nitrogen	vol. %	<10 ^b	<5 ^b		n.d./<5 ^b
Oxygen	vol. %	<3 ^b	<1 ^b		n.d./<1 ^b
Siloxanes ^c	mg/m ³	1.4–9.8 ^a	1.3 ^a	1.35 ^a	n.d. ^a
Sulphur	mg/m ³	29–900 ^a	<25 ^a	30 ^a	
Hydrogen sulfide	ppm	10–1000 ^b	150–3000		<30000/<5000 ^b
Ammonia	ppm	<5 ^a	<5 ^a	<5 ^a	<5 ^a
Halogenated compounds ^d	mg/m ³	0–7 ^a	n.d.	n.d.	<0.1 ^a
Benzene	mg/m ³	<36 ^e	<0.3 ^e		
Toluene	mg/m ³	<287 ^e	<12 ^e		

^a Arnold [4].

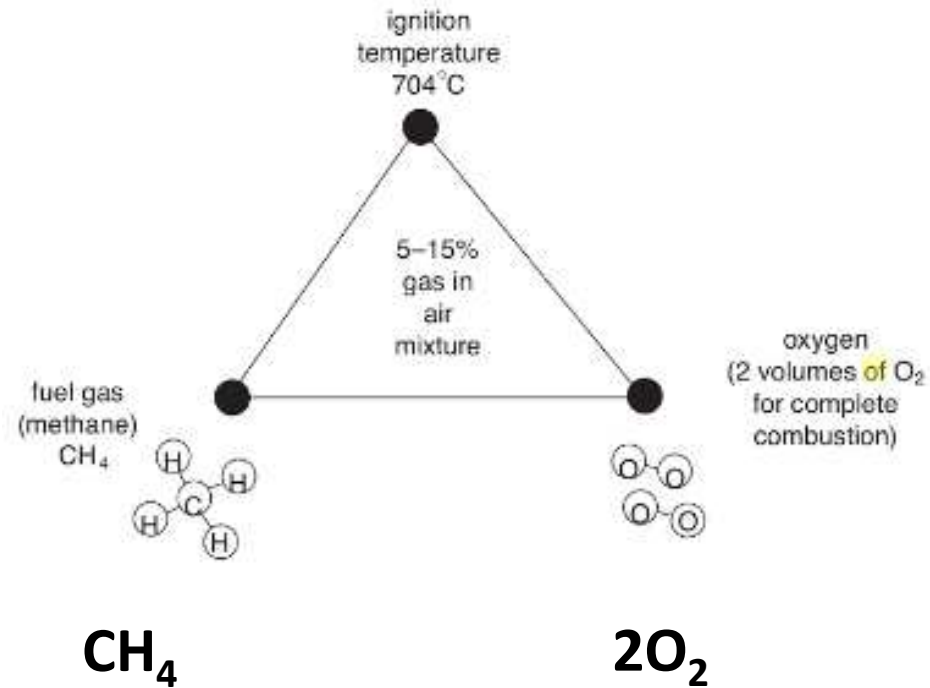
^b Oasmaa and Di Felipe [9].

^c L2–L4, D2–D4, TMS.

^d Quantified as toluene equivalent; n.d. = not detected.

^e Rasi et al. [10].

Methane combustion essentials



Stoichiometry

Natural gas interchangeability

Appliances
Boilers
Burners
Power plants
Turbines

heat release burner

Dimensionless
constant $\leftarrow = kd^2_0\sqrt{\Delta p}$

Hole diameter
of the burner $\leftarrow$

Heat release
throughout the hole $\leftarrow$

$$\left(\frac{HV\rho_{fu}}{\sqrt{\rho_{fu}}\sqrt{\rho_{air}}} \right)$$



Wobbe Index (WI)

Natural gas interchangeability

Appliances
Boilers
Burners
Power plants
Turbines

e.g. biogas



Family	Gas type	Approx. Wobbe no.
1st	Manufactured (town gas)	24–29
2nd	Natural	48–53
3rd	LPG	72–87

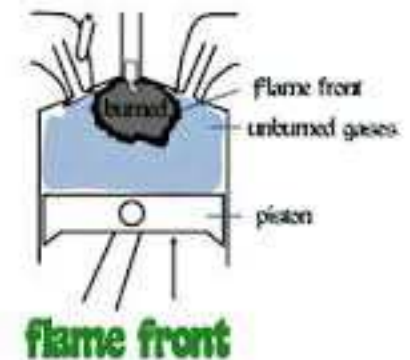
MJ/Nm³

Flame speed

Laminar

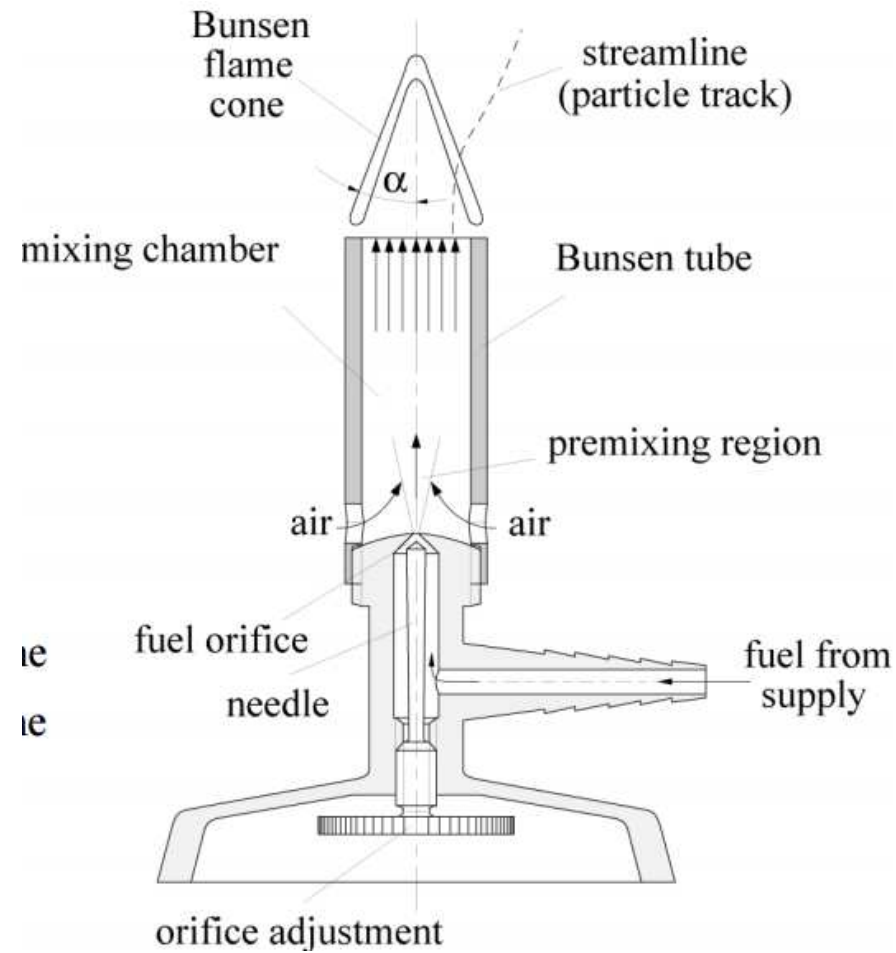
Turbulent

Pre-mixture



Difusion



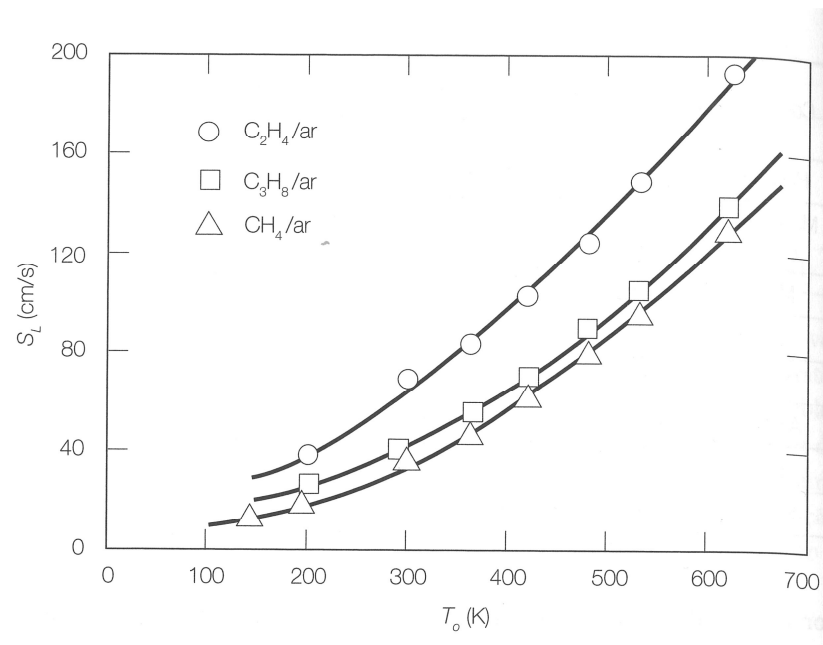


Laminar Flame Speed

$$SL \propto T^m$$

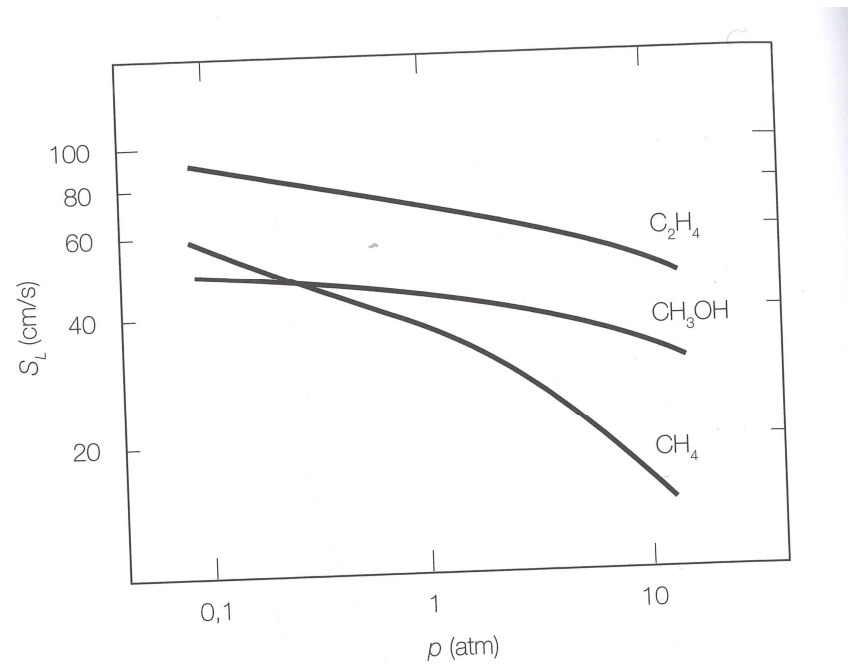


Reactants initial
temperature



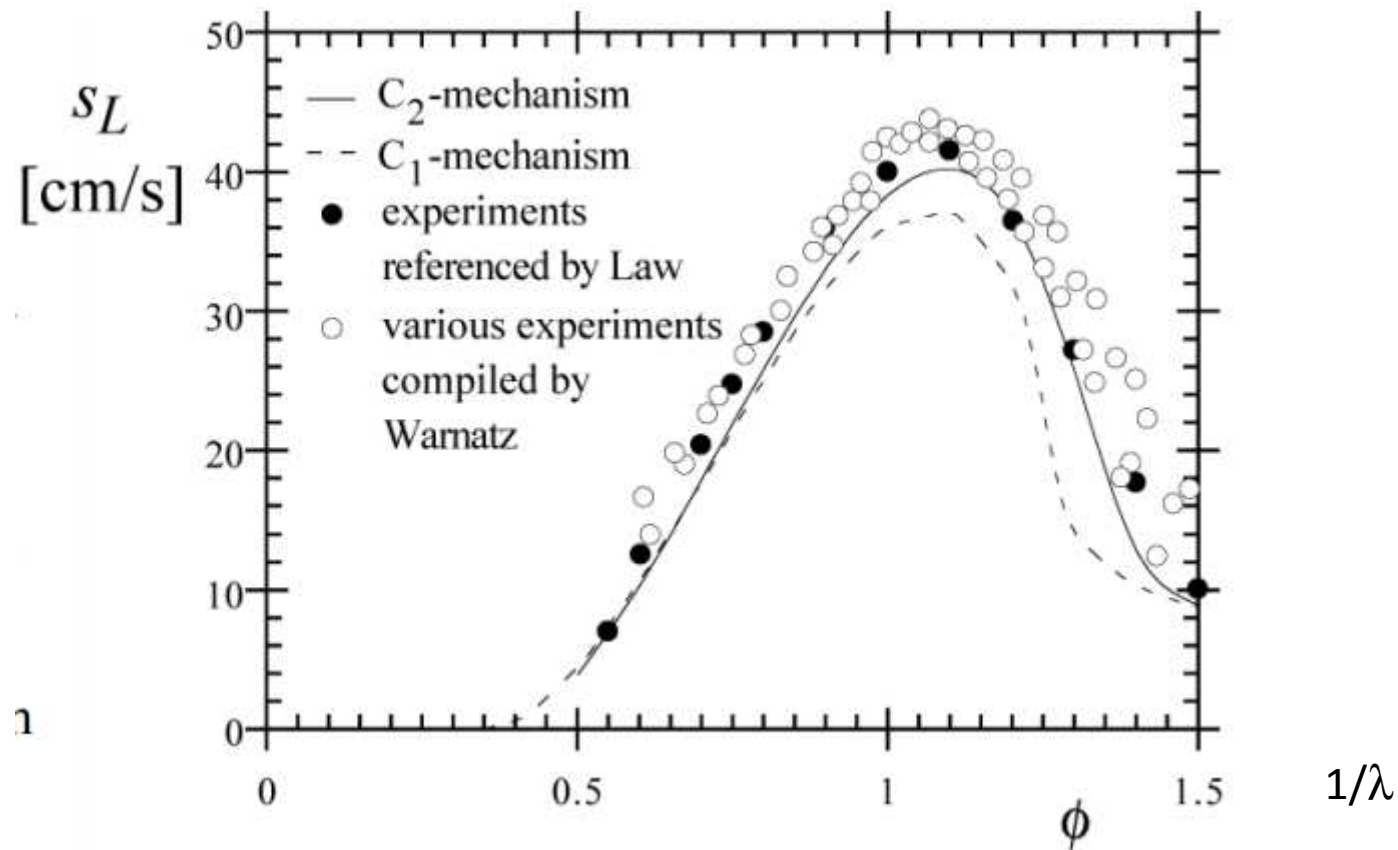
$$SL_{CH_4} \left(\frac{cm}{s} \right) = 10 + 3.71 \times 10^{-4} T^2$$

Laminar Flame Speed



$$SL_{CH_4} \left(\frac{cm}{s} \right) = 43p^{-0.5}$$

p em atm



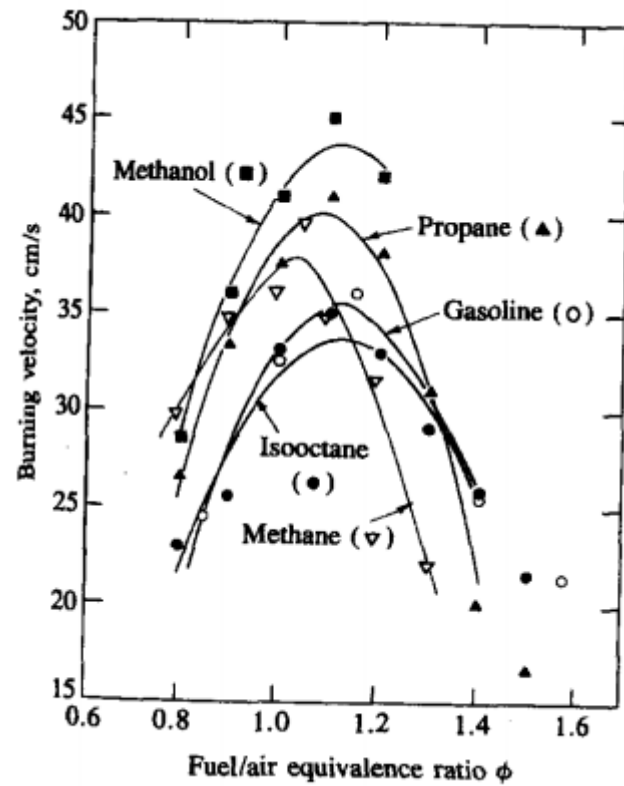
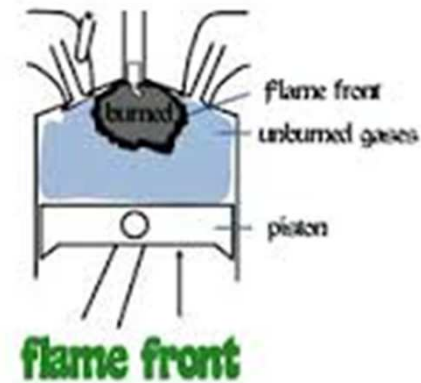


FIGURE 9-25

Laminar burning velocity for several fuels as function of equivalence ratio, at 1 atm and 300 K. Lines are least-squares polynomial fits to data.^{29, 30}



$$1/\lambda$$

$$S_L = S_{L,0} \left(\frac{T_u}{T_0} \right)^\alpha \left(\frac{p}{p_0} \right)^\beta \quad (9.33)$$

where $T_0 = 298$ K and $p_0 = 1$ atm are the reference temperature and pressure, and $S_{L,0}$, α , and β are constants for a given fuel, equivalence ratio, and burned gas diluent fraction. For propane, isooctane, and methanol, these constants can be represented by

$$\alpha = 2.18 - 0.8(\phi - 1) \quad (9.34a)$$

$$\beta = -0.16 + 0.22(\phi - 1) \quad (9.34b)$$

and

$$S_{L,0} = B_m + B_\phi(\phi - \phi_m)^2 \quad (9.35)$$

where ϕ_m is the equivalence ratio at which $S_{L,0}$ is a maximum with value B_m .

Parameters ϕ_m , B_m , and B_ϕ for Eq. (9.35)

Fuel	ϕ_m	B_m , cm/s	B_ϕ , cm/s	Ref.
Methanol	1.11	36.9	-140.5	30
Propane	1.08	34.2	-138.7	30
Isooctane	1.13	26.3	-84.7	30
Gasoline	1.21	30.5	-54.9	32

Note: Values of $S_{L,0}$ given by Eq. (9.35) are obtained from least-squares fits of Eq. (9.33) to data over the range $p = 1-8$ atm, $T_u = 300-700$ K. They do not correspond exactly to the laminar flame speed data at 1 atm and 298 K in Fig. 9-25.

$1/\lambda$

Metghalchi & Keck (1982)

$$S_L = S_{L,ref} \left(\frac{T_o}{T_{o,ref}} \right)^{\alpha_T} \left(\frac{p}{p_{ref}} \right)^{\alpha_p}$$

	$S_{L,ref}$ (m/s)	α_T	α_p
Metano ($\phi = 0,8$)	0,259	2,105	- 0,504
Metano ($\phi = 1,0$)	0,360	1,612	- 0,374
Metano ($\phi = 1,2$)	0,314	2,000	- 0,438
Propano ($0,8 \leq \phi \leq 1,5$)	$0,34 - 1,38 (\phi - 1,08)^2$	$2,18 - 0,8 (\phi - 1)$	$- 0,16 + 0,22 (\phi - 1)$

$1/\lambda$

Turbulence effect

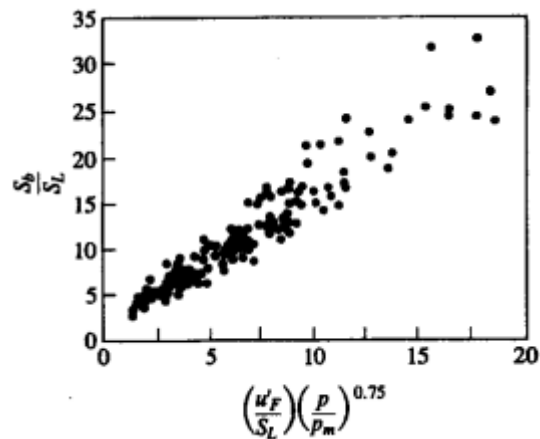
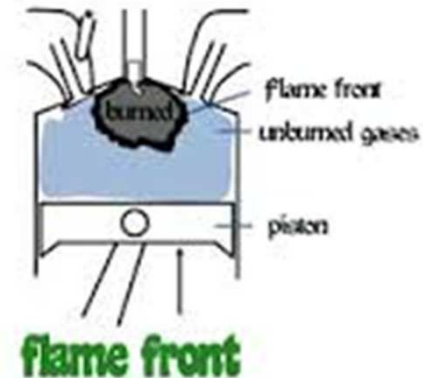
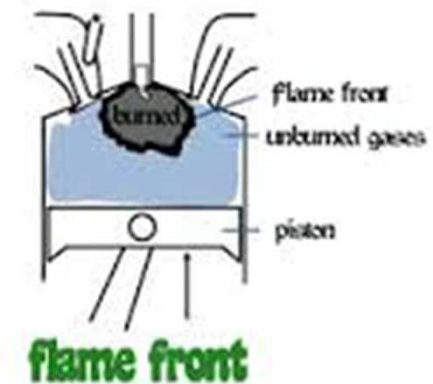
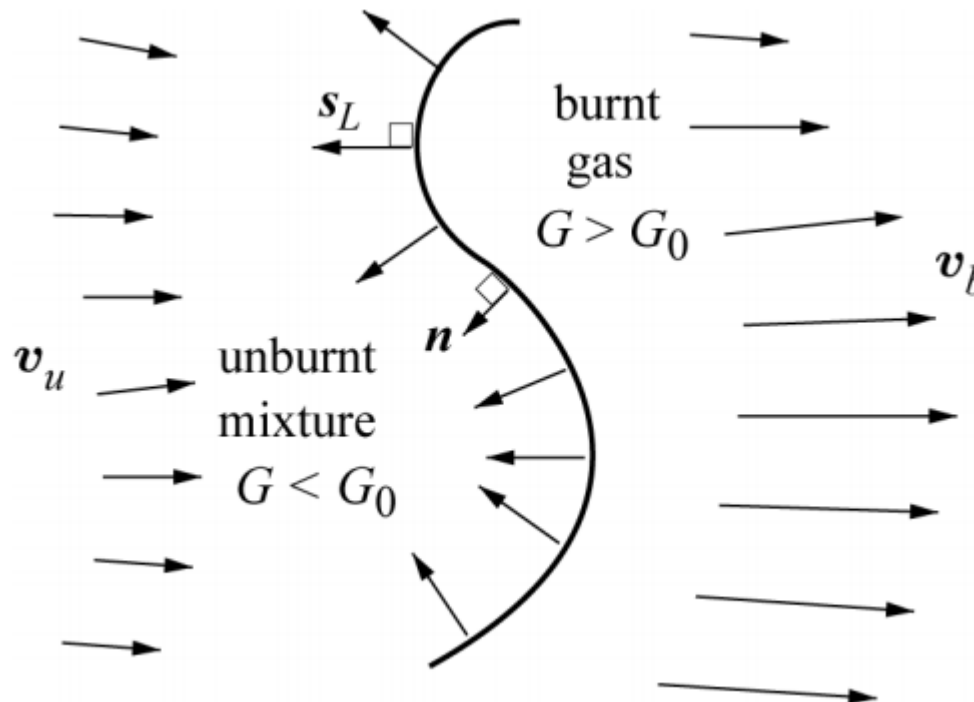


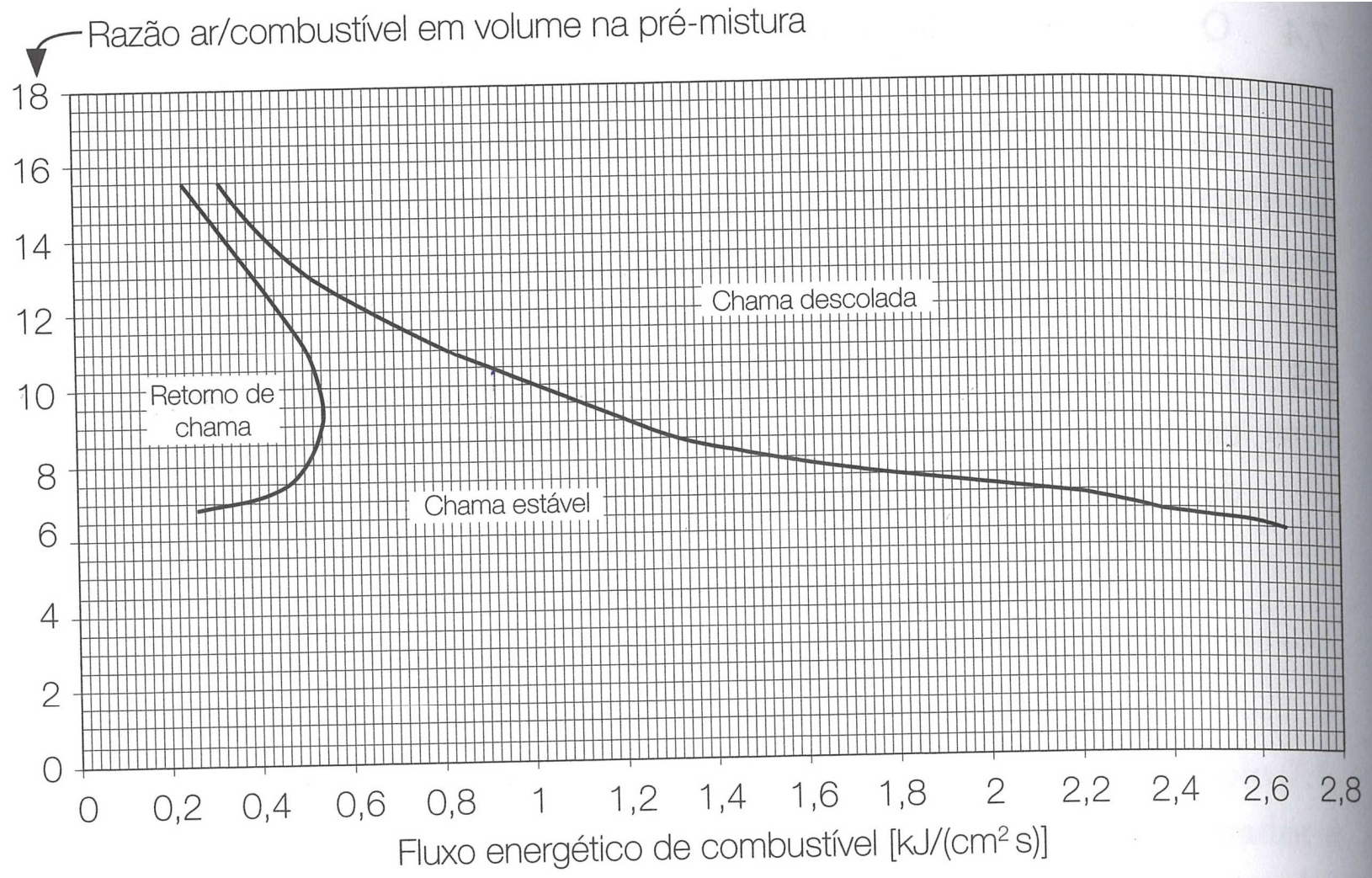
FIGURE 9-30

Variation of burning speed with turbulence intensity. The ensemble-averaged rms velocity fluctuation was measured during motoring engine operation. The ratio p/p_m (firing pressure/motoring pressure) corrects for the effect of additional compression on the turbulence intensity. Range of engine speeds and spark timings.³⁵



Laminar Flame Speed and reactants flow



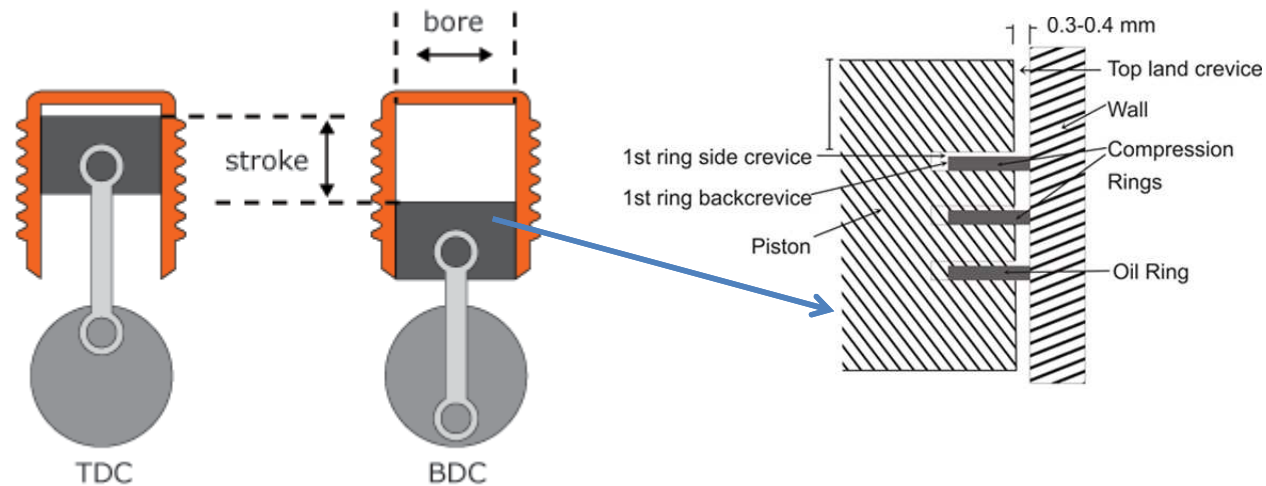


P#19 Pretende-se dimensionar os orifícios de um queimador que é alimentado com uma mistura de metano e ar à temperatura de 300 K e pressão de 100 kPa. O queimador tem de satisfazer a seguinte condição de funcionamento: potência calorífica fixa de 3 kW e mistura pobre ou estequiométrica. Não está previsto qualquer dispositivo de controlo automático e/ou de estabilização de chama. Considere um queimador com doze orifícios e procure maximizar a estabilidade das chamas.

- a) Escolha a composição da mistura e calcule o seu caudal.
- b) Dimencione os orifícios.

P#20 Imagine you are using LPG in a 4 cylinder, 1.4 liter internal combustion engine, compression ratio 12, bore=stroke. Assume a spherical centered flame front and cold start.

- LPG has a high octane number. Identify the type of combustion constant volume or constant pressure?
- Estimate the dimensions of the combustion chamber (assume bore=stroke).
- How much time do you estimate will be the combustion duration?
- Discuss HC (non-methane volatile organic compounds) formation near the oil rings where the temperature is 100°C.
- Repeat for a natural gas with high content of methane.

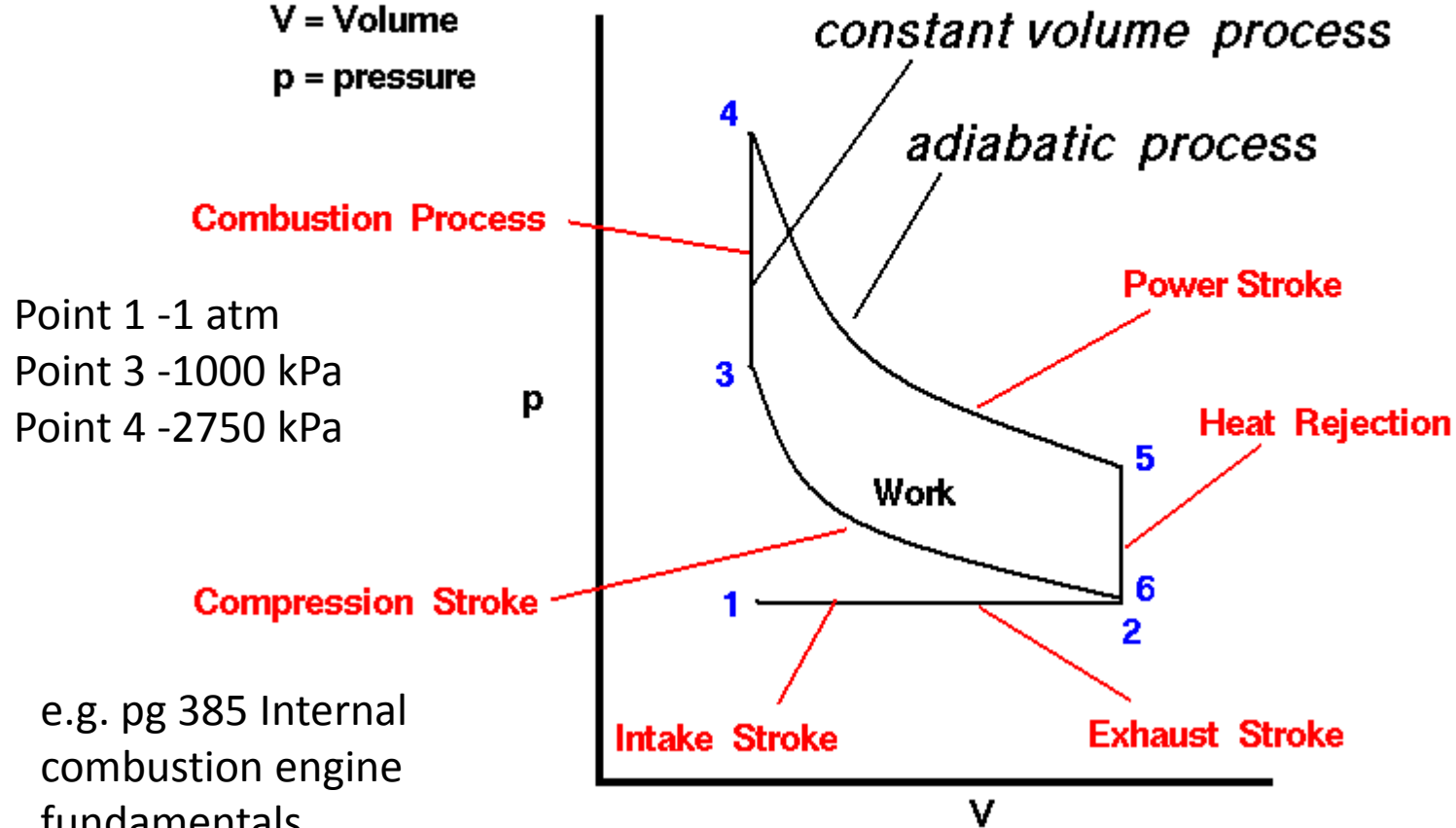




Ideal Otto Cycle *p-V diagram*

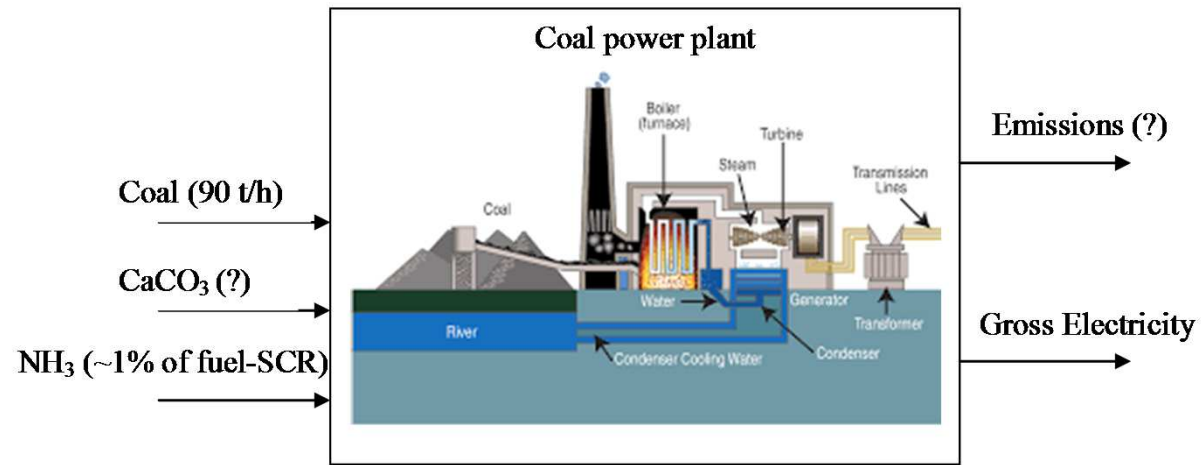
Glenn
Research
Center

V = Volume
p = pressure



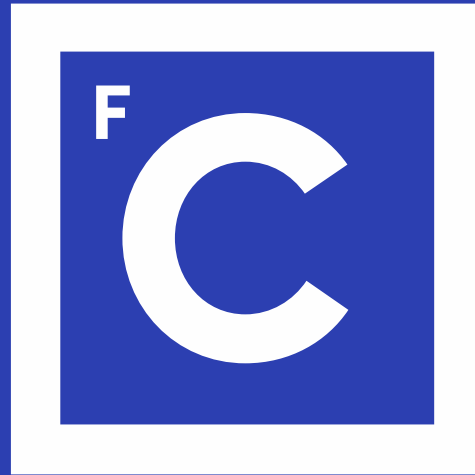
e.g. pg 385 Internal
combustion engine
fundamentals

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System operating pressure	21 ± 2 mbar	37 ± 5 mbar	28 ± 5 mbar
Liquid storage vapour pressure	–	6–7 bar	1.5–2 bar



The image consists of a large blue square. Inside this square is a white square, which is further enclosed by a smaller blue square. The word "Obrigado" is written in white, bold, sans-serif font in the center of the innermost blue square.

Obrigado



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